

## Wastewater treatment from potato processing industry using Moringa Oleifera-based coagulant

Potato is the third most important food crop on the planet. The potato processing industry produces a variety of food products and has high effluent generation with high organic load and solids content. These must be treated before being disposed of in water bodies. One of the options for treatment of industrial effluents widely studied in the literature is the use of natural coagulants. In this context, this work aims to evaluate the efficiency of effluent treatment of a potato processing industry in Brazil through the use of coagulants based on Moringa Oleifera. Five flocculation essays (Jar Essay) were performed, evaluating the use of Moringa Oleifera both in direct use (flour crushed) and in saline solution, for different coagulant mass and volume values. Turbidity removal rates close to 93% were obtained when using Moringa Oleifera in saline as a coagulant, which is the most efficient use of Moringa seeds compared to their direct use. BOD (Biochemical Oxygen Demand) removal was also high, with values around 90%. The Moringa planting area required for effluent treatment of the studied industry is 1.14 ha. The obtained results allowed the identification of the optimal coagulant dosages to be used and demonstrate the feasibility of using Moringa Oleifera to treat potato processing effluent.

**Keywords:** Moringa Oleifera; Potato processing industry; Effluent treatment; Coagulation; Flocculation.

## Tratamento de efluentes da indústria de processamento de batata usando coagulante à base de Moringa Oleifera

A batata é a terceira cultura alimentar mais importante do planeta. A indústria de processamento de batata produz uma variedade de produtos alimentícios e possui alta geração de efluentes com alta carga orgânica e teor de sólidos. Estes devem ser tratados antes de serem descartados em corpos d'água. Uma das opções para tratamento de efluentes industriais amplamente estudada na literatura é a utilização de coagulantes naturais. Nesse contexto, este trabalho tem como objetivo avaliar a eficiência do tratamento de efluentes de uma indústria processadora de batata no Brasil através do uso de coagulantes à base de Moringa Oleifera. Foram realizados cinco ensaios de floculação (Jar Essay), avaliando o uso da Moringa Oleifera tanto em uso direto (farinha triturada) quanto em solução salina, para diferentes valores de massa e volume de coagulante. Taxas de remoção de turbidez próximas a 93% foram obtidas ao usar Moringa Oleifera em solução salina como coagulante, que é o uso mais eficiente das sementes de Moringa em comparação ao seu uso direto. A remoção de BOD (Biochemical Oxygen Demand) também foi alta, com valores em torno de 90%. A área de plantio de Moringa necessária para tratamento de efluentes da indústria estudada é de 1,14 ha. Os resultados obtidos permitiram a identificação das dosagens ótimas de coagulante a serem utilizadas e demonstraram a viabilidade do uso da Moringa Oleifera no tratamento de efluente de processamento de batata.

**Palavras-chave:** Moringa Oleifera; Indústria de processamento de batata; Tratamento de efluentes; Coagulação; Floculação.

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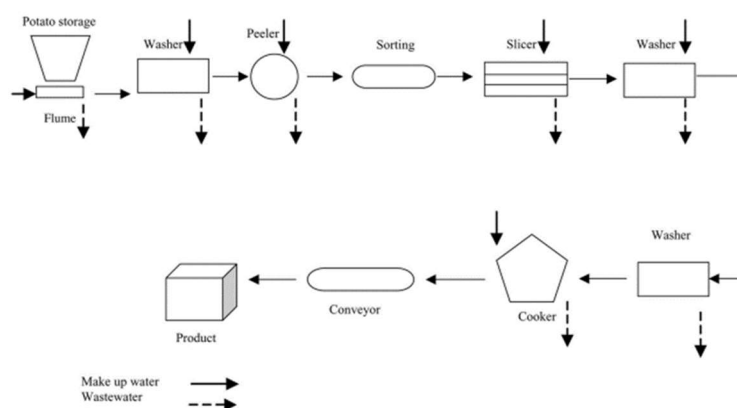
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## INTRODUCTION

The food industry has high levels of water consumption and effluent production per production unit (TIKARIHA et al., 2014). Among the various types of food industries, potato processing stands out. Potato (*Solanum tuberosum* L.) is the third most important food crop on the planet. It is estimated that over one billion people worldwide consume potatoes daily. Its annual world production exceeds 330 million tons in an area of 18 million hectares, and China and India are the main producers. The potato industry is a booming industry due to the versatility and composition of its products. Existing products include frozen and dehydrated, but it is the dehydrated grated potatoes and chips that are most marketed (CARVALHO, 2012).

In the Brazilian scenario, it is also of great importance and its productivity is on the rise, as both in natura and processed consumption increase. Currently the largest producing state in the Southeast is Minas Gerais, with southern Minas Gerais the largest planting area (AGRIANUAL, 2015). Like all industrial processes, the manufacture of grated potatoes and chips generates large amounts of waste, including potato peel, potato residual pulp and starch.

According to Moura (2013), in the processing of chips, water is widely used to wash the tubers from the beginning of the process until moments before the potato is sent to frying. A lot of water is used throughout the process, but the washing step after cutting is the most important, where the potato slices are washed with water jets or dipped to remove the starch released on the surface so to prevent them from sticking to each other during the frying process. In the case of grated potatoes, the washing process must be more careful, because there is greater starch release and the pieces are more fragile and more susceptible to breakage (TFOUNI et al., 2003). The figure 1 summarizes the process sequence of a conventional potato processing plant (HUNG et al., 2006). In this figure, we observe the need for water at various stages of the process. Water consumption varies depending on the type of product obtained from the potato, when it is between 11 - 22.55 l of water per kg of product (WALKER et al., 2018).



**Figure 1:** Scheme of a conventional potato processing plant. Source: Hung et al. (2006).

With intensive use of water in potato processing there is high generation of effluents. These effluents are characterized by a rich concentration of biodegradable compounds such as starch, proteins and also high suspended solids content (ZOUTBERG et al., 1999), with varying concentrations depending on the methods and the final processing product (HUNG et al., 2006). Therefore, several authors have studied the treatment

of these effluents from the potato processing industry.

Authors such as Hadjivassilis et al. (1997) and Zoutberg et al. (1999) investigated the use of anaerobic and/or aerobic reactors for potato processing effluent treatment and they obtained high chemical oxygen demand removal (COD) efficiency values. Kobya et al. (2006) obtained high values of electrocoagulation removal, achieving high COD removal efficiency and turbidity when using aluminum electrodes, consuming 4 kWh/m<sup>3</sup>. Makwana et al. (2016) also apply electrocoagulation as an aftertreatment to anaerobic reactors, obtaining high efficiency not only in the treatment of COD and turbidity, but also in the reduction of fecal and total coliforms and phosphate.

More sophisticated treatments have also been suggested recently. Silva et al. (2016) suggest an alternative treatment for potato processing effluent pretreatment using solid catalysts for mineralization through heterogeneous photo-Fenton process using discarded pile ferrite. The effluent photodegradation results obtained showed a 32% solution mineralization efficiency during the initial 10 minutes. The authors conclude that these are quite interesting for the use of this process as pretreatment to conventional treatments. Radeef et al. (2019) treat these effluents with energy recovery using microbiological fuel cells, obtaining 90% removal efficiency of 90%, with power of 97,5 W/m<sup>2</sup> in closed circuit.

One of the options for the sustainable treatment of industrial effluents is through natural product-based coagulants, such as *Moringa Oleifera* (MO) seed base (PAULA et al., 2014). Natural coagulants and flocculants, as MO (*Moringa Oleifera*), have shown advantages over chemicals, especially in relation to biodegradability and low production of residual sludge (MONACO et al., 2010). MO (*Moringa Oleifera*) is a perennial species of the Moringaceae family, originating from northeastern India (CORRÊA, 1984). It is a small tree, drought tolerant and fast growing, and adapts to a wide range of soils (CARDOSO et al., 2008). It is very hardy, grows in tropical warm and semi-arid climate at temperatures in the range of 25-35 °C, can withstand up to 48 °C for limited periods, and is drought tolerant (PRICE et al., 2000).

The coagulant action of MO (*Moringa Oleifera*) seed is due to the present fraction of high molecular weight cationic protein in its seeds, which causes destabilization of the particles contained in water and subsequent colloid coagulation (NDABIGENGESERE et al., 1995). These can be used directly in the form of flour or in aqueous, saline or more complex extracts, the coagulant extraction methodology and it is an influential treatment factor (VILLASEÑOR-BASULTO et al., 2018; ROCHA et al., 2019). However, Madrona et al. (2012) found that the protein concentration in the coagulant solution increases as the saline concentration increases. According to Valverde et al. (2013), MO (*Moringa Oleifera*), unlike metal-based chemical coagulants, acts over a large pH range and does not significantly change the pH of treated water. MO (*Moringa Oleifera*) has several other applications besides coagulant effect, such as food source and medicinal function, industrial use for obtaining biodiesel oil and agronomic use (RANGEL, 1999; LIU et al., 2018; FERNANDES et al., 2019). Oil obtained from seeds has no toxic effects (KAYODE et al., 2015).

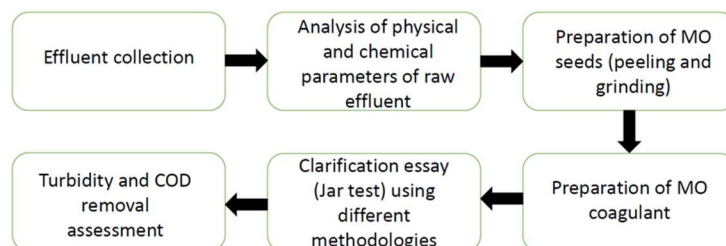
Studies of MO (*Moringa Oleifera*) applications for industrial effluent treatment are abundant in the literature, including treatment of dairy effluent, distilleries, textile industries, heavy metals, food industry, among others, and a complete review on the subject can be obtained in Villaseñor-Basulto et al. (2018).

However, no studies are found in the literature for the effluent treatment of the potato processing industry using MO (*Moringa Oleifera*).

In this context, the objective of the present work is to evaluate the efficiency of MO-based coagulants in the treatment of turbidity and effluent COD (Chemical Oxygen Demand) from the potato processing industry, under different coagulant preparation and dosage methodologies. Comparison with traditional commercial coagulants such as ferric chloride and aluminum sulfate are also performed. Finally, the required planting area and the technical feasibility of applying *Moringa Oleifera* in a potato processing industry in Brazil is discussed.

## METHODOLOGY

As it was previously mentioned, the coagulant used in the treatment is organic based and was produced by using *Moringa Oleifera* seeds in direct application and use in saline solution. There are no applications in literature so far of the use of *Moringa Oleifera* for treatment of this type of effluent. Figure 2 briefly shows the steps for performing the experiments in this article. The main steps in this figure are presented in later topics. After evaluation of the treatment efficiency, an estimate of the necessary planting area for the application of MO (*Moringa Oleifera*) seeds for effluent treatment of a potato processing industry was performed.



**Figure 2:** Flowchart of laboratory steps.

### Effluent collection and characterization

The effluent used for this experiment comes from the potato processing industry of the city of Maria da Fé, located in the south of Minas Gerais state, Brazilian state with the largest potato production. Although sparsely populated (14.646 inhabitants), the city has a preponderance in potato processing and has seven factories. The correct treatment of these effluents is essential to minimize the impact on the environment.

In all, 5 trials were carried out with a total consumption of 50 liters of effluent, and this volume does not belong to the same sampling day, varying according to the potato processing days and laboratory dates. The essays were performed at the Sanitation Laboratory of the Federal University of Itajubá, Brazil. For the initial characterization of the effluent, the measurement methodologies presented in Standard Methods for Examination for the Examination of Water and Wastewater (APHA, 2012) were followed. Table 1 indicates the procedure used to determine the parameters.

**Table 1:** Physicochemical parameters measured in the samples.

Parameters	Methodology
pH	PH reading by pH meter (Model: Digimed DM - 220 V)
Turbidity	Turbidity Reading by Digital Turbidity Meter (Model: PoliControl AP2000)
Conductivity	Conductivity Reading by Conductivity Meter
COD	1.5 ml K <sub>2</sub> Cr <sub>2</sub> O <sub>7</sub> was added; 3.5 ml H <sub>2</sub> SO <sub>4</sub> and 2.5 ml sample. The sample was taken to the digester for 2 hours at 150 ° C and then it was read on the spectrophotometer.
BOD (Biochemical Oxygen Demand)	The dissolved oxygen concentration (initial OD) in the sample was measured. Then the sample was sealed and kept in an oven for five days at 20 ° C in an amber vial and the pH adjusted to neutral. At the end of the five days, the measurement of dissolved oxygen (final DO) was repeated. BOD (Biochemical Oxygen Demand) was given by the difference between the initial OD and the final OD

### Preparation of MO (*Moringa Oleifera*) and Coagulant Seeds

In the experiments of this work, coagulants prepared from MO (*Moringa Oleifera*) seed were used in two forms: crushed (direct use) and in saline solution. According to Arantes et al. (2012), MO (*Moringa Oleifera*) flour with a small particle size, reduces some lipids that are present in seeds, also reducing turbidity and apparent color when flour is used in water treatment processes. The procedure for applying this alternative was as follows: i) Seed husk removal; ii) Store in an oven at 150°C for 24 hours for drying; iii) Crushing the seeds with the support of a mixer for 15 minutes; and iv) Maintaining seeds in a desiccator.

The preparation of the MO (*Moringa Oleifera*) solution in saline solution was adapted from the methodology applied by Madrona et al. (2012), applying the following procedure: i) Preparation of a 1 mol/L NaCl solution; (ii) Weighing of crushed and blended *Moringa Oleifera* pasta; (iii) homogenization of seed powder with 100 ml of saline solution; iv) Rest of solution for 24 hours.

From the fourth essay two commercial coagulants were used to compare with the natural coagulant, aluminum sulfate (Al<sub>2</sub>(SO<sub>4</sub>)<sub>3</sub>) and ferric chloride (FeCl<sub>3</sub>).

### Coagulation Essay Methodology (Jar Test)

Five Jar Tests were performed to evaluate the efficiency of coagulation and flocculation in the effluent treatment. In each of the trials, five 1.5 L effluent jars and different coagulant volumes were used. Table 2 presents the methodology and the main aspects of each of the essays studied. Table 2 shows that the methodology composition in the different essays was quite diverse and several parameters were varied from one essay to another, or even within a single essay in the different jars employed. This resulted from the fact that the application proposed by the authors has been innovative in the literature so far, seeing that the information on which the authors could base their studies was scarce, leading the authors to define the condition of each new essay based on the results of the previous study, in order to find the best coagulant preparation methodology as well as to improve its coagulant dosage.

For the first four essays the following coagulation parameters were applied in the Jar Test: i) Rapid Mixing: Rotation of 200 RPM for 60 seconds; ii) Slow Mix: 100 RPM rotation for 40 minutes; and iii) Sedimentation: 60 minutes for sediment deposition (same parameters applied by VIEIRA et al., 2009; JUNHO

et al., 2021). In order to achieve greater efficiency, higher values of coagulation parameters used in the treatment of high organic wastewater were applied to the fifth essay. The values for this essay were: i) Rapid Mix: 480 RPM rotation for 60 seconds; ii) Slow Mix: Spin at 54 RPM for 10 minutes; iii) Sedimentation: 20 minutes for sediment deposition.

**Table 2:** Summary of the methodology applied to each essay.

Essays	Coagulant Type	Mass or volume of coagulant in each jar	Justification
I	MO ( <i>Moringa Oleifera</i> ) ground into flour	Jar1: 0,5 g of coagulant	The MO ( <i>Moringa Oleifera</i> ) masses used in each jar were arbitrarily chosen, initially taking lower values in order to understand the effluent behavior with the addition of the coagulant mass.
		Jar2: 0,75 g of coagulant	
		Jar 3: 1 g of coagulant	
		Jar4: 1,5 g of coagulant	
		Jar5: 2 g of coagulant	
II	MO ( <i>Moringa Oleifera</i> ) in saline that was prepared using 3g of seed	Jar1: 10 ml of coagulant	The increase of the crushed MO ( <i>Moringa Oleifera</i> ) mass in relation to the previous essay was performed aiming to analyze an optimal maximum value of efficiency in this type of application. Saline MO ( <i>Moringa Oleifera</i> ) was also tested with arbitrarily determined increasing coagulant volumes
		Jar2: 20 ml of coagulant	
		Jar3: 30 ml of coagulant	
	MO ( <i>Moringa Oleifera</i> ) ground into flour	Jar4: 3 g of coagulant	
	The jar was not used	-	
III	MO ( <i>Moringa Oleifera</i> ) in saline solution that was prepared using 6g of seed	Jar 1: 40 ml of coagulant	Third essay: adaptation of the second essay, seeking greater efficiency in results by greater use of mass and seeds.
		Jar 2: 60 ml of coagulant	
	MO ( <i>Moringa Oleifera</i> ) was ground into flour	Jarro 3: 8 g of coagulant	
	The jars were not used	-	
IV	Use of Commercial Ferric Chloride Coagulant ( $\text{FeCl}_3$ )	Jar 1: 7,5 ml of coagulant	From the fourth trial, we sought to verify the effectiveness of conventional treatment with coagulants based on MO ( <i>Moringa Oleifera</i> ), also evaluate the use of commercial coagulants and compare which has greater efficiency in treatment.
		Jar 2: 11,25 ml of coagulant	
	MO ( <i>Moringa Oleifera</i> ) ground into flour	Jar 3: 16 g of coagulant	
	The jar was not used	-	
V	MO ( <i>Moringa Oleifera</i> ) in saline solution using 15 g of seeds, filtered using 40 [ $\mu$ ] sheet paper and correcting the pH of the solution until reaching pH 7.0	Jarro 1: 50 ml of coagulant	The filtration to remove moringa powder residues in saline solution was performed to verify the influence of these residues on the treated effluent turbidity. The potato effluent has a more acidic pH, so it was decided to leave the neutral pH by adding sodium hydroxide (NaOH) (10 g/l), in order to improve the treatment efficiency. Another commercial coagulant, besides ferric chloride was evaluated, aluminum sulfate. In this last essay, BOD (Biochemical Oxygen Demand) and COD (Chemical Oxygen Demand) were also analyzed.
		Ferric chloride ( $\text{FeCl}_3$ )	
	Jar 3: 22.5 ml of coagulant		
	Aluminum sulfate ( $\text{Al}_2(\text{SO}_4)_3$ )	Jar 4: 18.75 ml of coagulant	
	The jar was not used	-	

## Estimated MO (*Moringa Oleifera*) planting area required to service a potato processing plant in Brazil

In order to analyze the planting area and mass of MO (*Moringa Oleifera*) seeds that will be spent to attend the effluent treatment of the potato processing plant from which the samples were collected, it was adopted a yield of MO (*Moringa Oleifera*) seed production by tree with 24 kg/year (*Moringa* Brazil, 2012) and a number of trees per hectare of 2000 (AYERZA, 2012). These are the same values used by Rocha et al. (2019). The effluent production from the industry assessed is approximately 30,000 l/d, with 20 production days per month. The mass of MO (*Moringa Oleifera*) seed consumed in kg/year was calculated based on the mass per l of sample used to prepare the saline solution for the highest turbidity removal essay.

## RESULTS AND DISCUSSION

### Laboratory results

The table 3 indicates the initial characteristics of the raw effluent for the samples used in each of the five essays, respectively. It is noteworthy that the samples were not collected on the same day, which justifies the differences in their characteristics.

**Table 3:** Initial characteristics of the analyzed effluent.

Parameter	Sample 1	Sample 2	Sample 3	Sample 4	Sample 5	Average
pH at 25°	5.44	5.39	5.65	5.18	5.54	5.54 ± 0.18
Turbidity (NTU- Nephelometric Turbidity Unity)	570	483	521	573	1101	649.6 ± 255.1
Conductivity (mS/cm)	1.69	2.24	3.81	5	2.31	3.01 ± 1.37

It can be seen from table 3 that the pH of the sample is generally acidic. There is also a high turbidity variation between the first 4 samples and the last one, which may be explained by a higher solids loading in the washed potatoes on this day. Table 4 indicates the results obtained in the first trial.

**Table 4:** First Essay: Final Result of Treated Effluent.

Jars	Moringa mass used in g	Final pH	Final Turbidity in NTU (Nephelometric Turbidity Unity)	Turbidity Removal Efficiency	Final Conductivity in mS/cm
Jar 1	0.5	5.53	519	8.95%	4.85
Jar 2	0.75	5.61	502	11.93%	4.71
Jar 3	1	5.63	331	41.93%	2.06
Jar 4	1.5	5.68	318	44.21%	1.91
Jar 5	2	5.69	295	48.25%	1.91

From the results obtained, regarding turbidity, it can be concluded that the MO (*Moringa Oleifera*) powder masses used were not the most effective for the treatment of this effluent, seeing that the removal efficiency for none of the 5 jars was if above 50%. Jar 5, which used the highest MO (*Moringa Oleifera*) mass, was the one that obtained the largest turbidity reduction, which indicates the need for a higher MO (*Moringa Oleifera*) mass.

As for the pH, as expected, the MO (*Moringa Oleifera*) tends not to modify it, keeping in the same range of the initial value, and the small changes in the pH occurred with the gradual increase of the moringa

mass. The effluent temperature, before and after the addition of *Moringa*, remained between 25°C and 26°C, so it can be said that for these concentrations, the *moringa* does not remove or print heat in the solution that acts. Conductivity was high in all jars, especially those with low turbidity removal efficiency, probably due to the absence of coagulation reaction.

The Table 5 presents the results of the second essay. It was tested, in addition to the higher mass MO (*Moringa Oleifera*) flour, the MO (*Moringa Oleifera*) in saline prepared using 3g MO (*Moringa Oleifera*) (see table 2). It is noted that all essays were able to obtain high turbidity removal values, with percentages above 50%. The saline solution had a higher turbidity removal, explained by the fact that the *moringa*'s particles were more dissolved and in smaller flakes, allowing for the most efficient coagulation process. The highest turbidity removal efficiencies were in the use of Saline Solution (30 ml - Jar 3).

**Table 5:** Second Essay: Final Result of Treated Effluent.

Jars	Coagulant Items	Coagulant mass/volume	Final pH	Final Turbidity in NTU (Nephelometric Turbidity Unity)	Turbidity Removal Efficiency	Final Conductivity in mS/cm
Jar 1	Saline solution in ml	10	5.42	101	79.09%	2.63
Jar 2		20	5.43	96	80.12%	2.79
Jar 3		30	5.45	85	82.40%	3.06
Jar 4	MO ( <i>Moringa Oleifera</i> ) ground in g	5	5.55	140	71.01%	4.55

Again, the pH of the sample did not change at the end of the process and its temperature remained at approximately 25°C, which characterizes an advantage of MO (*Moringa Oleifera*). The conductivities in the saline samples increased with increasing volume, and the conductivity in the crushed MO (*Moringa Oleifera*) direct use sample was the highest among all worked. This can be explained by the diameter and particle composition of *Moringa* powder. The favorable results from the second essay indicate that an increased use of MO (*Moringa Oleifera*) may lead to even more positive results, which led to the completion of the third trial.

Table 6 sets out the results obtained in the third trial. This maintained the same logic as the second trial, comparing the use of MO (*Moringa Oleifera*) in saline, now more concentrated and prepared 6g seed (double from the previous trial), and used directly ground.

**Table 6:** Third Essay: Final Result of Treated Effluent.

Jar s	Coagulant Items	Coagulant mass/volume	Final pH	Final Turbidity in NTU (Nephelometric Turbidity Unity)	Turbidity Removal Efficiency	Final Conductivity in mS/cm
Jar 1	Saline solution in ml	40	5.69	90	82.73%	5.9
Jar 2		60	5.67	89	82.92%	6.54
Jar 3	Moringa in g	8	5.71	74.2	85.76%	4.38

For the third trial, all jars showed more than 80% turbidity removal, but the sample from Jar 3, with direct use of crushed MO (*Moringa Oleifera*) was the most efficient. For saline MO (*Moringa Oleifera*), there is a small increase in efficiency, around 0.19%, between jars 1 and 2, despite the large increase in the volume



of coagulant used (20 ml or 50%) and a certain increase conductivity of the sample. This indicates a stabilization trend, that is, the use of more concentrated solutions or larger volumes will not lead to high turbidity removal gains. The direct use of moringa powder is still efficient, with increasing percentage of turbidity removal between masses of 5 g (second essay - 71%) and 8 g (85% - third essay), which demonstrates that unlike saline, MO (*Moringa Oleifera*) still does not tend to stabilize. The pH remained in the same range as the initial pH, as expected, and the temperature did not vary, as in the other essays.

The results obtained in all three demonstrate the effectiveness of the effluent treatment of the potato processing industry from MO (*Moringa Oleifera*), both in saline and crushed powder. It is noteworthy that although consuming a higher amount of gm of MO (*Moringa Oleifera*) seed, direct use in 8g was more efficient than the use of saline solution with 6g of MO (*Moringa Oleifera*) and not consuming water or salt in the preparation of coagulant.

Subsequent trials (4 and 5) focus on comparing the good results already obtained with MO (*Moringa Oleifera*) coagulants with those of commercial coagulants. Essay 4 compared the use of ferric chloride with direct use of MO (*Moringa Oleifera*) with twice the mass used in essay 3, seeing that no tendency to stabilize turbidity removal in this type of coagulant was observed. The results of the fourth trial are presented by Table 7.

**Table 7:** Fourth Essay: Final Result of Treated Effluent.

Jars	Coagulant items	Coagulant mass/volume	Final pH	Final Turbidity in NTU (Nephelometric Turbidity Unity)	Turbidity Removal Efficiency	Final Conductivity in mS/cm
Jar 1	FeCl <sub>3</sub> in ml	7.5	5.09	566	1.22%	4.89
Jar 2		11.25	5.12	555	3.14%	4.66
Jar 3	Moringa in g	16	5.03	900	-57.07 %	4.78

This essay was the one that presented the lowest efficiency with regard to Turbidity removal. Ferric Chloride concentrations taken from Silva et al. (2007) methodology proved ineffective for coagulation. In addition, the direct application of Moringa, evident in jar3, with a mass of MO (*Moringa Oleifera*) equal to twice the previous essay, eventually increased the turbidity of the sample, by reason of being present in an excessive concentration which inhibited the coagulation reaction and increased the concentration of suspended solids in the effluent. Thus a value (16 g) was found for which it was no longer recommended to use the direct application of Moringa powder.

The table 8 shows the results obtained in the fifth and last trial. In this trial, the MO (*Moringa Oleifera*) coagulant was compared with two commonly used commercial coagulants in Brazil, ferric chloride (normally used for sewage treatment) and aluminum sulfate (used for water treatment). As aluminum sulfate has its optimal operation near neutral pH, the pH was adjusted in all samples. We know that the authors had already come to a conclusion regarding the use of direct MO (*Moringa Oleifera*) in trials 3 and 4, this essay was performed with more concentrated saline (15 g of MO - *Moringa Oleifera*) carefully filtered to remove any residual MO (*Moringa Oleifera*) dust (see table 2). The coagulant volume used was the intermediate between the optimal volumes identified in essay 3.

**Table 8:** Fifth Essay: Final Result of Treated Effluent.

Jars	Coagulant Items	Concentration	Final pH	Final Turbidity in NTU (Nephelometric Turbidity Unity)	Turbidity Removal Efficiency	Final Conductivity in mS/cm
Jar 1	FeCl <sub>3</sub> in ml	18.75	6.79	560	49.14%	2.55
Jar 2		22.5	6.73	699	36.51%	2.58
Jar 3	Saline solution in ml	50	6.96	70	93.64%	2.2
Jar 4	Al <sub>2</sub> (SO <sub>4</sub> ) <sub>3</sub> in ml	18.75	6.67	311	71.75%	2.31

It can be seen from table 8 that turbidity removal efficiency was less than 80% in all use cases of commercial metal based coagulants. Only in the case of saline solution was obtained a removal efficiency greater than 90%, the highest value obtained in the present work. This behavior can be explained by the following factors: saline filtration, change in coagulation parameters or greater initial turbidity of sample 5 (see table 2).

The addition of FeCl<sub>3</sub> formed a by-product that changed the effluent shade to a dark green to black color. This byproduct may be the result of a reaction between the Iron chloride chloride ion and a dissociated sodium metabisulfite ion (Na<sub>2</sub>S<sub>2</sub>O<sub>5</sub>), an inorganic compound released in the preparation of potato chips with antioxidant/preservative function, forming a by-product of bronze color tending to black. Another explanation is that Ferric Chloride may have been released at a higher concentration than the effluent dilution capacity, because FeCl<sub>3</sub> prepared as a coagulant also has a dark color, characteristic of Iron, and it is an insoluble compound in organic solvents, the contact of a high concentration with the starch present in the effluent, and it may have caused the generation of dark colored byproducts.

Seeing that this was the highest turbidity removal efficiency essay, the COD (Chemical Oxygen Demand) removal efficiency of the coagulation process was also evaluated (Table 9). While the commercial coagulants showed no efficiency of removal of these parameters, the efficiency of removal of organic load of the saline solution of MO (*Moringa Oleifera*) was high, presenting values above 80% for both BOD (Biochemical Oxygen Demand) and COD (Chemical Oxygen Demand), which characterizes it as a viable treatment option from the potato processing industry. This value complies with Resolution 430/2011 of the National Environmental Council (CONAMA, 2011) which stipulates a minimum BOD (Biochemical Oxygen Demand) reduction efficiency of 70% for effluent disposal in Brazilian water sources.

**Table 9:** Fifth Essay: COD (Chemical Oxygen Demand) and BOD (Biochemical Oxygen Demand) for Raw and Treated Effluent.

Jars	Coagulant Items	Initial COD (Chemical Oxygen Demand) in mg/l	Final COD (Chemical Oxygen Demand) in mg/L	COD (Chemical Oxygen Demand) removal efficiency	Initial BOD (Biochemical Oxygen Demand) in mg/l	Final BOD (Biochemical Oxygen Demand) mg/l	BOD (Biochemical Oxygen Demand) Removal Efficiency
Jar 1	FeCl <sub>3</sub> in ml	2580	2450	5%	1747	N/A	N/A
Jar 2		2580	2670	-3%	1747	N/A	N/A

J a r 3	Saline solution in ml	2580	468	82%	1747	188	89%
J a r 4	Al <sub>2</sub> (SO <sub>4</sub> ) <sub>3</sub> in ml	2580	2030	21%	1747	N/A	N/A

Due to the large number of essays evaluated, a summary of the essays that showed a turbidity reduction of 80% or more is presented in table 10. From the analysis of the results of this table, it can be concluded that many of the tested alternatives presented technical viability for be applied in a potato processing company. It is also observed in this table that using a lower mass of MO (*Moringa Oleifera*) and a lower energy expenditure with rotation, it was also possible to reach high values of efficiency. An example that proved to be quite satisfactory was the one obtained by using the moringa in direct application referring to essay 3, where it was possible, with a smaller amount of moringa mass, lower expenses with solution and energy preparation for clarification processes almost 86% removal was obtained. The fifth trial, even though it had the highest removal efficiency, used a higher MO (*Moringa Oleifera*) mass, requiring even a larger tree planting area to meet the treatment demand and requiring higher energy expenditure with the Fast and Slow Mixing process.

**Table 10:** General Summary of the highest efficiency essays.

Essay	Coagulant	Coagulant Volume/Mass ml	MO ( <i>Moringa Oleifera</i> ) mass in coagulant preparation	Turbidity Removal Efficiency	Methodology
2	Saline solution in ml	10	3	80.12%	Fast Mix: 200 RPM for 1 min; Slow Mix: 100 RPM for 40 minutes
		20		82.40%	
3	Saline solution in ml	40	6	82.73%	
		60		82.92%	
	MO ( <i>Moringa Oleifera</i> ) ground in g	8	-	85.76%	
5	Saline solution in ml	50	15	93.64%	

### MO (*Moringa Oleifera*) planting area required for application in a potato processing industry

Table 11 presents the results of seed mass, number of trees and cultivation area needed to meet the demand for effluent treatment of the potato processing plant from which the effluents were collected, in Maria da Fé, Minas Gerais.

**Table 11:** MO (*Moringa Oleifera*) Required Planting.

Required Moringa Mass	54750	kg/year
Number of trees	2281.25	Trees
Planting Area	11406.25	m <sup>2</sup>

It was found that the small value of required area obtained, is just over 1 ha (1.14 ha). The cost of land for planting in Brazil varies between 1,000 and 10,000 USD/ha, demonstrating that investments for planting MO (*Moringa Oleifera*) for coagulant production in the industry studied are not high. As previously explained, the city studied has 7 potato processing factories producing a variety of products, which indicates

the possibility of a joint plan between the owners of the city's factories for joint planting of MO (*Moringa Oleifera*) even assisted by the municipal public agency, seeking to act as an environmental compensation to the city, repairing the environmental damage caused by its actions. The sludge generated by the treatment via MO (*Moringa Oleifera*) is biodegradable and can be used on the MO (*Moringa Oleifera*) plantations themselves. Third party investment for seed production for coagulant production and sale to factories is also a plausible option that can become a vector of income, jobs and development in the still-dependent city and region.

## CONCLUSIONS

The present document evaluated the efficiency of the potato processing industry effluent treatment using *Moringa Oleifera*-based coagulants. Several combinations of coagulant preparation modes, MO (*Moringa Oleifera*) concentration and coagulant volume were tested to obtain the best treatment to be applied in a real factory.

Several essays showed high turbidity reduction, and one of the main uses is the use of 8 g of crushed *Moringa* seed (86% turbidity removal) and 50 ml saline prepared with 15 g of seed, passing the solution through the filter and correcting the pH of the samples (93% of turbidity removal), and the first option consumes approximately half of the seeds required for saline preparation. In the case of saline solution, the removal of BOD (Biochemical Oxygen Demand) and COD (Chemical Oxygen Demand) was above 80%, a value that meets the minimum reduction values established by Brazilian legislation (60%). The commercial iron and aluminum based coagulants tested showed no efficiency in the effluent treatment.

The application of MO (*Moringa Oleifera*) for treatment of effluents from the processing industry of the studied coat requires a small area (just over 1 ha), which makes it possible to plant MO (*Moringa Oleifera*) for coagulant production. Due to the large number of potato processing factories in the city studied (7), several opportunities could arise from planting MO (*Moringa Oleifera*) for the city, such as partnerships between city hall and industries, job creation, income and improved water bodies quality.

The wide diversity of essays and methodologies provides a comprehensive database for decision making and application of MO (*Moringa Oleifera*) coagulants in potato processing industries, not only in factories in the region studied, but around the world. Especially in developing countries dependent on the agricultural sector, such as Brazil, the use of MO (*Moringa Oleifera*) coagulants may be a good option for low cost treatment of solid and organic material effluents from the potato processing industry without pH change of the final effluent, contributing to the water quality of the springs of these countries, generating also a biodegradable sludge that can be used as fertilizer.

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